# ARTICLE OPEN (Reck for updates) High-throughput computational-experimental screening protocol for the discovery of bimetallic catalysts

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To accelerate the discovery of materials through computations and experiments, a well-established protocol closely bridging these methods is required. We introduce a high-throughput screening protocol for the discovery of bimetallic catalysts that replace palladium (Pd), where the similarities in the electronic density of states patterns were employed as a screening descriptor. Using first-principles calculations, we screened 4350 bimetallic alloy structures and proposed eight candidates expected to have catalytic performance comparable to that of Pd. Our experiments demonstrate that four bimetallic catalysts indeed exhibit catalytic properties comparable to those of Pd. Moreover, we discover a bimetallic (Ni-Pt) catalyst that has not yet been reported for H<sub>2</sub>O<sub>2</sub> direct synthesis. In particular, Ni<sub>61</sub>Pt<sub>39</sub> outperforms the prototypical Pd catalyst for the chemical reaction and exhibits a 9.5-fold enhancement in cost-normalized productivity. This protocol provides an opportunity for the catalyst discovery for the replacement or reduction in the use of the platinum-group metals.

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## INTRODUCTION

One of the important roles of computer simulations in materials science is to predict and/or design materials prior to experiments. In particular, first-principles calculations using density functional theory (DFT) have played a vital role in the field of catalysis<sup>1–3</sup>. The computational framework enables the prediction or understanding of reaction pathways on catalyst surfaces, which is undoubtedly useful for experimentalists. However, the accurate estimation of some crucial properties such as the reaction barriers on catalytic surfaces is extremely time-consuming in first-principles calculation schemes. In this regard, obtaining a full understanding of the catalytic reaction mechanism via first-principles calculations is often considered rather inefficient. In our experience, although dependent on computing power, a time cost of several months is required for computing a full energetics picture of even one metallic catalyst system. The efficiency of the search of catalysts via first-principles calculations has therefore been questioned because carrying out experimental tests without the aid of computer simulations can often be even faster.

To maximize the efficiency of catalyst discovery using combined computational and experimental studies, the descriptors or features that bridge these two areas should be wisely chosen. Specifically, a simple but physically reasonable descriptor or feature enabling the representation of catalytic properties is critical. A representative example of such a descriptor is the *d*-band center theory that correlates between the *d*-band center<sup>4</sup>, i.e., the average energy of electronic *d*-states projected onto a surface atom of the catalyst, and the gas adsorption energy, which is widely accepted in the field of metallic catalysis. Coupled with the volcano relationship between catalytic activity and adsorption energy<sup>5</sup>, it is theoretically possible to predict catalytic activity from the *d*-band center without exploration of the full reaction

mechanism. Later, along with the *d*-band center theory, consideration of the *d*-band shapes describing higher moments of the *d*-band as well as the *sp*-band properties describing local Pauli electronegativity were also suggested to capture the surface reactivity of transition metal alloys<sup>6–8</sup>. These studies indicate that the electronic density of states (DOS) patterns themselves projected onto the surface atoms of catalysts can serve as an improved descriptor for the development of metal catalysts because they include more comprehensive information on not only *d*-states but also *sp*-states (both their values and shapes). Nonetheless, the full DOS patterns themselves have never been used as a descriptor in combined computational-experimental screening processes.

As electronic structures are key to determining the physical/ chemical properties of materials, materials with similar electronic structures tend to exhibit similar properties. Indeed, a DFT study revealed that a solid-solution  $Ir_{50}Au_{50}$  alloy can exhibit catalytic properties for the H<sub>2</sub> dissociation reaction with an activity comparable to that of Pt, and this result is attributed to the similar electronic structures (DOS patterns) of the Ir<sub>50</sub>Au<sub>50</sub> alloy and Pt<sup>9</sup>. In another example, the similar electronic structures of  $Rh_{50}Ag_{50}$  and Pd were experimentally verified for hydrogen storage<sup>10</sup>. The similar electronic structural characteristics enable the Rh<sub>50</sub>Ag<sub>50</sub> alloy to exhibit hydrogen storage properties superior to those of Pd<sup>11</sup>, although neither Rh nor Ag alone shows hydrogen storage properties<sup>9</sup>. Thus, bimetallic alloys with a DOS pattern similar to that of Pd, which is a well-known representative metal catalyst, should exhibit catalytic performance similar to that of Pd, which is a good hypothesis for the high-throughput development of bimetallic catalysts.

Here, we used the full DOS pattern as a key descriptor in highthroughput computational-experimental screening protocols. As a



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demonstration in the high-throughput search of bimetallic catalysts, we selected palladium (Pd), the prototypical catalyst for hydrogen peroxide (H<sub>2</sub>O<sub>2</sub>) synthesis from hydrogen (H<sub>2</sub>) and oxygen  $(O_2)$  gases<sup>12–14</sup>, as our reference material. Using DFT calculations, we first screened 4350 crystal structures of bimetallic alloys to investigate their thermodynamic stabilities (only closestpacked surfaces were considered). Next, the similarities in the DOS patterns between the alloys and Pd were quantified, and subsequently, their synthetic feasibility was evaluated. Through these processes, we finally proposed eight candidates with high DOS similarities with Pd, which are expected to show catalytic properties comparable to those of Pd. These eight screened alloys were experimentally synthesized and tested for H<sub>2</sub>O<sub>2</sub> direct synthesis, and four of them (Ni<sub>61</sub>Pt<sub>39</sub>, Au<sub>51</sub>Pd<sub>49</sub>, Pt<sub>52</sub>Pd<sub>48</sub>, and Pd<sub>52</sub>Ni<sub>48</sub>) indeed exhibited catalytic properties comparable to those of Pd. In particular, Pd-free Ni<sub>61</sub>Pt<sub>39</sub> is greatly outperformed prototypic Pd with a 9.5-fold enhancement in cost-normalized productivity (CNP) owing to the high content of inexpensive Ni.

## RESULTS

# High-throughput computational screening for bimetallic catalysts

Figure 1 shows a schematic diagram of our high-throughput screening protocol for the discovery of bimetallic catalysts. Based on 30 transition metals in periods IV, V, and VI, we considered a total of 435  $(_{30}C_2)$  binary systems with a 1:1 (50:50) composition. For each alloy combination, 10 ordered phases that are available for 1:1 composition were investigated, namely, B1, B2, B3, B4, B11, B19, B27, B33, L1<sub>0</sub>, and L1<sub>1</sub>, leading to a screening of 4350 (435  $\times$ 10) crystal structures. Using DFT calculations, we calculated the formation energy ( $\Delta E_{\rm f}$ ) of each phase and determined which crystal structure is most stable in the bulk phase. Here, negative formation energy implies that the phase is thermodynamically favorable (or that the element combination is miscible), and vice versa. Because nonequilibrium alloyed phases can be stabilized by the nanosize effect, although the elemental combinations are immiscible in the bulk phases<sup>11,15,16</sup>, a margin of  $\Delta E_{\rm f} < 0.1$  eV was considered when screening the thermodynamic stabilities of the bimetallic systems. The alloyed structures with  $\Delta E_f > 0.1 \text{ eV}$  could be readily synthesized; however, such structures would be easily transformed into phase-separated structures during chemical reactions (two-phase structures of the pure elements), which is not suitable for their practical uses as catalysts. Eventually, a total of 435 binary systems and 249 alloys were filtered at the thermodynamic screening step.

For the 249 thermodynamically screened alloys, we calculated the DOS pattern projected on the close-packed surface for each structure and compared it with that of the Pd(111) surface. To quantitatively compare the similarity of two DOS patterns, we defined the following measure:

$$\Delta DOS_{2-1} = \left\{ \int [DOS_2(E) - DOS_1(E)]^2 g(E;\sigma) dE \right\}^{\frac{1}{2}}$$
(1)

$$g(E;\sigma) = \frac{1}{\sigma\sqrt{2\pi}} e^{-\frac{(E-E_{\rm F})^2}{2\sigma^2}}$$
(2)

Here,  $\Delta DOS_{2-1}$  in Eq. (1) indicates the similarity between the DOS of the alloy (DOS<sub>2</sub>) and the DOS of the reference Pd(111) (DOS<sub>1</sub>) in which a Gaussian distribution function,  $g(E; \sigma)$  in Eq. (2) is considered to compare the two DOS patterns near Fermi energy ( $E_F$ ) with the high weight. We set the standard deviation,  $\sigma = 7 \text{ eV}$  because most of the *d*-band centers for the bimetallic alloys are distributed from -3.5 eV to 0 eV relative to the Fermi energy.

In comparing two DOS patterns, both *d*-states and *sp*-states were considered. To clarify the importance of the inclusion of *sp*-states, we discuss this effect with an example of  $O_2$  adsorption on

 $Ni_{50}Pt_{50}(111)$ , which is one of the elementary steps for  $H_2O_2$  direct synthesis. In Fig. 2, the DOS patterns for *d*-states and *sp*-states are shown; the patterns are obtained by the sum of the partial DOSs of the surface Ni and Pt atoms on Ni<sub>50</sub>Pt<sub>50</sub>(111). Comparing the DOS patterns before/after O<sub>2</sub> adsorption, the change in the *d*band DOS is negligible after O<sub>2</sub> adsorption. On the other hand, the sp-band DOS patterns change more smoothly after O<sub>2</sub> adsorption. This result implies that an  $O_2$  molecule interacts more with the *sp*bands of the surface Ni and Pt atoms than with the *d*-bands on Ni<sub>50</sub>Pt<sub>50</sub>(111) in O<sub>2</sub> adsorption. The partial DOSs of O<sub>2</sub> before/after  $O_2$  adsorption on Ni<sub>50</sub>Pt<sub>50</sub>(111) are also compared in Fig. 2. An  $O_2$ molecule in the gas phase has a pair of half-occupied orbitals ( $\pi_{n}^{*}$ ) in a triplet state, which leads to magnetic properties, resulting from the spin-splitting into up and down states. After O<sub>2</sub> adsorption, the orbitals of the O2 molecule broaden and the spin-splitting character disappears. Thus, the magnetic moment of the adsorbed O<sub>2</sub> becomes zero (peroxo state), which is supportive evidence that the  $\pi_{p}^{*}$  states are fully occupied through the interaction between the metal surface atoms and the O<sub>2</sub> molecule. Then, orbital hybridization between the sp-states of the Ni<sub>50</sub>Pt<sub>50</sub> surface and the *p*-states of the O<sub>2</sub> molecule mainly occurs, therefore, consideration of the DOS patterns including the sp-state is required, at a minimum, for H<sub>2</sub>O<sub>2</sub> direct synthesis.

The DOS similarity values of the 249 alloy surfaces are shown in Fig. 3. According to the definition of the DOS similarity, as the value approaches zero, the electronic structure of the alloy becomes more similar to that of Pd(111), and the material is expected to show catalytic properties similar to those of Pd(111). In Fig. 3, we chose 17 candidates with the low DOS similarity values ( $\Delta DOS_{2-1} < 2.0$ ): CrRh ( $\Delta DOS_{2-1} = 1.97$ , B2 structure), FeCo (1.63, B2), CoNi (1.71, L1<sub>0</sub>), CoHf (1.89, L1<sub>0</sub>), CoTa (1.96, L1<sub>0</sub>), CoPt (1.78, L1<sub>0</sub>), NiCu (1.11, L1<sub>0</sub>), NiNb (1.96, L1<sub>0</sub>), NiMo (1.87, L1<sub>0</sub>), NiRh (0.98, L1<sub>0</sub>), Ni-Pd (0.84, L1<sub>0</sub>), Nilr (1.28, L1<sub>0</sub>), Ni-Pt (1.16, L1<sub>0</sub>), CuPd (1.51, B2), RhPt (1.67, L1<sub>0</sub>), Pd-Pt (1.16, L1<sub>0</sub>), and PdAu (1.43, L1<sub>0</sub>). Here, owing to the rarity of Hf and Ta, the CoHf and CoTa alloys were excluded from the candidate list. In addition, we excluded NiCu and CrRh from the list because the large reduction potential difference between the elements in the binary system leads to the unfavorable formation of alloyed structures in which the two elements are homogeneously mixed via a wet-chemical method for nanoparticle (NP) synthesis<sup>17</sup>.

# Experimental verification of the DFT-guided bimetallic catalysts

For the remaining 13 candidates, we tried to synthesize their alloyed NPs and confirm whether their crystal structures were identical to those (Fig. 3) predicted by DFT calculations. For NP synthesis, we used a butyllithium reduction method<sup>18</sup>. Details of the NP synthesis are found in the Methods section. Because it was assumed in Fig. 3 that the proposed alloys had a composition of 50:50, we intended to synthesize alloys with nearly the same composition. Inductively coupled plasma (ICP) analyses revealed that the compositions of the synthesized alloys (loading ratio of metal precursors = 50:50) were  $Au_{51}Pd_{49}$ ,  $Ni_{61}Pt_{39}$ ,  $Pd_{50}Cu_{50}$ , Pd<sub>52</sub>Ni<sub>48</sub>, Pt<sub>58</sub>Co<sub>42</sub>, Pt<sub>52</sub>Pd<sub>48</sub>, Rh<sub>56</sub>Ni<sub>44</sub>, and Rh<sub>56</sub>Pt<sub>44</sub>; however, CoFe, Nilr, NiMo, NiNb, and NiCo were not alloyed because the reducing power of butyllithium used as a reducing agent was likely insufficient. To confirm whether the alloyed NPs had the same crystal structures as predicted by DFT, their X-ray powder diffraction (XRD) patterns were investigated, as shown in Fig. 4. The samples showed alloyed diffraction patterns without signals from phases of the pure elements that compose each alloy. We also simulated XRD patterns of the alloys on the basis of the DFT crystal structures and found that the simulated patterns matched well with the experimental patterns. This result clearly reveals that we successfully synthesized alloyed NPs with the crystal structures predicted by DFT calculations for eight bimetallic systems. The



# **Promising catalyst** < 10 candidates

Fig. 1 High-throughput screening protocol for the discovery of bimetallic catalysts. There are three screening steps to identify catalyst candidates from 4350 candidates. The top (cyan color) section indicates the first step showing 30 elements and 10 crystal structures to collect binary alloys with a 1:1 composition. The middle (magenta color) and bottom (violet color) sections indicate the second and the last steps relevant to the thermodynamic stability and the DOS similarity, respectively.

lattice parameters for the alloyed samples are presented in Supplementary Table 1. In addition, we performed Rietveld refinements of the XRD patterns (Supplementary Figure 1). The synthesized NPs clearly have cubic-based structures as predicted by our DFT calculations, although in the Ni-Pt samples a small amount of non-alloyed Pt (pure Pt) coexists with alloyed Ni<sub>72</sub>Pt<sub>28</sub>. As we used the synthesized Ni-Pt samples themselves when measuring their catalytic performance, we used the ICP composition (Ni<sub>61</sub>Pt<sub>39</sub>).

It was also important to determine whether the synthesized NPs have ordered or disordered structures because the two types of structures can show different catalytic properties<sup>19</sup>. The main role of our descriptor ( $\Delta DOS_{2-1}$ ) in the high-throughput protocol for catalyst development is to discover potential catalysts and then transfer the information to experimentalists at high speed. For this purpose, a reference structure for comparison with alloys is required because various structures are possible for random solid-solution structures. In this work, ordered structures were used as a reference and were also validated by comparing simulated and



**Fig. 2 Partial DOS for the Ni**<sub>50</sub>**Pt**<sub>50</sub> (111) **system before and after O<sub>2</sub> adsorption.** The *s*-states (light), *p*-states (dark), and *d*-states (patterned) DOS plots are shown. Occupied states are filled in color; unoccupied states are depicted by lines. **a**–**c** The shape of states without adsorbed O<sub>2</sub> on the Ni<sub>50</sub>Pt<sub>50</sub> (111) surface and O<sub>2</sub> gas phase in a vacuum. **d**–**e** The shape of states of the Ni<sub>50</sub>Pt<sub>50</sub> (111) surface and O<sub>2</sub> of the adsorbed system.

experimental XRD patterns. From this process, we intended to predict the possibilities and tendencies of alloys for use as  $H_2O_2$  direct synthesis catalysts. Nevertheless, because the synthesized sample could include random solid-solution structures, there is the potential for discrepancies between theory and experiment.

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We further characterized the NP samples by high-angle annular dark-field scanning transmission electron microscopy (Fig. 4 and Supplementary Figure 2~9). The elemental color mapping and overlay clearly indicate the homogeneous mixing of elements in each NP. The mean diameters of the alloyed NPs were  $3.4 \pm 0.4$  nm (Pd<sub>50</sub>Cu<sub>50</sub>),  $8.8 \pm 2.0$  nm (Ni<sub>61</sub>Pt<sub>39</sub>),  $5.0 \pm 1.5$  nm (Rh<sub>56</sub>Ni<sub>44</sub>),  $11.6 \pm 2.0$  nm (Au<sub>51</sub>Pd<sub>49</sub>),  $5.2 \pm 1.5$  nm (Pd<sub>52</sub>Ni<sub>48</sub>),  $8.1 \pm 2.2$  nm (Pt<sub>52</sub>Pd<sub>48</sub>),  $5.8 \pm 1.0$  nm (Pt<sub>58</sub>Co<sub>42</sub>), and  $1.7 \pm 0.2$  nm (Rh<sub>56</sub>Pt<sub>44</sub>). In particular, for the four alloys (Ni<sub>61</sub>Pt<sub>39</sub>, Au<sub>51</sub>Pd<sub>49</sub>, Pd<sub>52</sub>Ni<sub>48</sub>, and Pt<sub>52</sub>Pd<sub>48</sub>) showing catalytic properties comparable to those of Pd (Table 1), their NP diameters were in the range of  $5.2\sim11.6$  nm, which is similar to the diameter ( $7.2 \pm 1.6$  nm) of Pd NPs (Supplementary Figure 10).

To investigate whether the catalytic performance of the eight proposed alloys is comparable to that of Pd, the alloyed catalysts were tested for direct H<sub>2</sub>O<sub>2</sub> synthesis under mild conditions (20°C, 1 atm) in comparison to pure Pd (Table 1). Along with the industrial importance of H2O2 as an eco-friendly oxidizing agent<sup>20,21</sup>, the  $H_2O_2$  direct synthesis reaction can be performed under ambient temperature and pressure conditions, and Pd has been regarded as the archetypical catalyst for the chemical reaction although there is still room for performance enhancement<sup>22</sup>. In terms of  $H_2O_2$  productivity representing the catalytic activity for  $H_2O_2$  direct synthesis, three alloy systems,  $Au_{51}Pd_{49}$  (505.2 mmol<sub>H2O2</sub> gmetal<sup>-1</sup> h<sup>-1</sup>), Ni<sub>61</sub>Pt<sub>39</sub> (880.1), and Pt<sub>52</sub>Pd<sub>48</sub> (1225.6) exhibited performance comparable to that of Pd (552.4). In addition, Pd<sub>52</sub>Ni<sub>48</sub> showed noticeable H<sub>2</sub>O<sub>2</sub> productivity (218.1), although this productivity is lower than that of Pd. Here, it is notable that the four alloy systems have lower  $\Delta DOS_{2-1}$  values than the alloy systems showing poor catalytic activities. Although the Rh-Ni system has a low  $\Delta DOS_{2-1}$  value, the DOS patterns near  $E_{\rm F}$  are quite different from those of Pd (Supplementary Figure 11), which can explain why it shows poor catalytic activity.

On the other hand, the orders of the  $\Delta DOS_{2-1}$  values and H<sub>2</sub> conversion do not show perfect consistency. However, it is not enough to represent the catalytic performance for H<sub>2</sub>O<sub>2</sub> direct synthesis only with  $H_2$  conversion. The  $H_2O_2$  synthesis reaction involves several elementary steps on the catalyst, such as H<sub>2</sub> dissociation and the first and second hydrogenation of O<sub>2</sub> generating OOH and H<sub>2</sub>O<sub>2</sub>, respectively. Moreover, when assessing the catalytic performance, side reactions such as H<sub>2</sub>O formation should be considered. In other words, the catalytic performance of H<sub>2</sub>O<sub>2</sub> direct synthesis is not dominated by only one catalytic behavior but coupled with multiple behaviors that involve not only H<sub>2</sub> conversion but also H<sub>2</sub>O<sub>2</sub> productivity and selectivity. In addition, we compared our descriptor of DOS similarity ( $\Delta DOS_{2-1}$ ) with the *d*-band center that has been widely used in metallic catalysts. Here, we considered the difference between the *d*-band centers of the alloys and that of Pd ( $|\varepsilon_{d,Pd} - \varepsilon_d|$ ); the *d*-band centers of the bimetallic alloys are shown in Supplementary Table 4. For comparison, Pt<sub>52</sub>Pd<sub>48</sub> and Pd<sub>50</sub>Cu<sub>50</sub> were chosen because they show relatively high and low H<sub>2</sub> conversions, respectively (Table 1). The  $\Delta DOS_{2-1}$  values appropriately represent the order of H<sub>2</sub> conversion (Pt<sub>52</sub>Pd<sub>48</sub>:  $\Delta DOS_{2-1} = 1.16$  and  $Pd_{50}Cu_{50}$ :  $\Delta DOS_{2-1} = 1.51$ ), in contrast to the difference in *d*-band centers (Pt52Pd48: 0.31 and Pd50Cu50: 0.08). In this regard, the similarity in DOS patterns can be a good descriptor for the discovery of bimetallic catalysts and needs no calculations relevant to the reaction pathways on the catalyst surfaces, which would require a high computational cost.

Among the four alloy combinations showing high  $H_2O_2$  productivity, the Au-Pd<sup>13,14,23–25</sup>, Ni-Pd<sup>26</sup>, and Pd-Pt<sup>27</sup> systems were previously reported as promising candidates for  $H_2O_2$  direct synthesis, validating our approach once again. In addition, our approach led to the discovery of a catalyst, a Ni-Pt alloy, which has not yet been reported for  $H_2O_2$  direct synthesis, although the system is well known as an oxygen reduction reaction (ORR) catalyst in fuel cells<sup>28–30</sup>. As the price of Pd rapidly increases<sup>31</sup>, our



**Fig. 3** Map of the thermodynamic stabilities and DOS similarities of bimetallic alloy systems. The diagonal components denote the most thermodynamically stable crystal structures (e.g., FCC, BCC, HCP, and SC) of pure metals. The occupied components under the diagonal denote the most thermodynamically stable crystal structures (e.g., B2, B11, B19, B27, B33, L1<sub>0</sub>, and L1<sub>1</sub>) of bimetallic alloys. The background colors above the diagonal describe the formation energies, and the occupied components above the diagonal denote the DOS similarity of each alloy compared with Pd(111).

Pd-free Ni-Pt alloy can serve as a more cost-effective option. To identify the cost-effectiveness of the Ni-Pt catalyst, we list the CNP (unit,  $mmol_{H2O2}$  \$metal<sup>-1</sup> h<sup>-1</sup>)<sup>32</sup> of the assessed materials in Table 1, in which the metal price [unit, U.S. dollar (\$)] instead of catalyst mass is used. In terms of this metric, N<sub>i61</sub>Pt<sub>39</sub> shows a CNP of 69.3, which is not only ~9.5 times higher than that of Pd (7.3) but also much higher than those of the other candidates (Au<sub>51</sub>Pd<sub>49</sub>: 7.1, Pd<sub>52</sub>Ni<sub>48</sub>: 5.5, and Pt<sub>52</sub>Pd<sub>48</sub>: 23.0). As another metric for catalytic activity, we also considered the turnover frequency of the catalysts. In terms of this metric,  $\mathrm{Ni}_{61}\mathrm{Pt}_{39}$  (98.5) shows a performance superior to that of Pd (58.8). Moreover, for efficient  $H_2O_2$  direct synthesis, the  $H_2$  conversion and  $H_2O_2$  selectivity properties of the catalysts should be considered. It is also interesting that Ni<sub>61</sub>Pt<sub>39</sub> shows an H<sub>2</sub>O<sub>2</sub> selectivity similar to that of Pd, although  $Ni_{61}Pt_{39}$  shows higher  $H_2$  conversion. These findings clearly demonstrate that the Ni-Pt bimetallic catalyst is very attractive for H<sub>2</sub>O<sub>2</sub> direct synthesis.

When screening bimetallic catalysts by electronic structure calculations, only one composition (50:50) for the bimetallic systems was considered because DFT prediction to determine the optimized composition to provide the best catalytic performance would be challenging and time-consuming. Instead, composition optimization proceeded with the help of experiments, likely providing a faster result than a DFT prediction. Therefore, to optimize the composition of the Ni-Pt bimetallic catalysts, we also explored the effects of the Ni/Pt ratio in Ni\_xPt\_{100-x} NPs on their catalytic properties for  $H_2O_2$  direct synthesis (Supplementary Table 2), and no significant structural changes in the Ni\_xPt\_{100-x} NPs were observed (Supplementary Figure 12 and 13). We found that the best catalytic performance was exhibited by Ni<sub>61</sub>Pt<sub>39</sub> in terms of  $H_2O_2$  productivity,  $H_2$  conversion, and  $H_2O_2$  selectivity.

#### **Catalytic reaction mechanism**

The Ni-Pt bimetallic catalysts were proposed based only on electronic structure calculations without any calculations relevant to the reaction pathways. Thus, to justify the experimental catalytic activity shown in Table 1, we investigated the reaction mechanisms on the catalyst surface using DFT calculations. We considered the close-packed (111) surface of the Ni<sub>50</sub>Pt<sub>50</sub> slab in  $L1_{0}$ , where the alloy composition was considered for simplicity of the calculations although the best catalytic performances were experimentally observed for the Ni<sub>61</sub>Pt<sub>39</sub> composition. The Langmuir-Hinshelwood mechanism<sup>33-35</sup> involving adsorption of both H<sub>2</sub> and O<sub>2</sub> over a catalyst surface was first explored. Our DFT calculations revealed that dissociative adsorption of H<sub>2</sub> occurs very favorably over Ni<sub>50</sub>Pt<sub>50</sub>(111) surfaces (Supplementary Figure 14), which is similar to Pd(111)<sup>33,34</sup>. This finding implies that the hydrogenation of O<sub>2</sub> over Pd(111) and Ni<sub>50</sub>Pt<sub>50</sub>(111) determines the catalytic activity for  $H_2O_2$  synthesis. In Fig. 5a, the overall  $H_2O_2$ synthesis involving two sequential hydrogenations of  $O_2$  (I $\rightarrow$ II and II $\rightarrow$ III) is exothermic by 0.42 eV on Ni<sub>50</sub>Pt<sub>50</sub>(111), which is more favorable than the value of 0.07 eV for Pd(111). Moreover, while the rate-determining step on Pd(111) is the first hydrogenation  $(I \rightarrow II)$  to form OOH\* (\*denotes a surface site) with an energy barrier of 0.78 eV, the rate-determining step on Ni<sub>50</sub>Pt<sub>50</sub>(111) is observed at the desorption step of the generated  $H_2O_2^*$ , with an energy barrier of 0.69 eV (III $\rightarrow$ V). These results indicate that higher  $H_2O_2$  productivity is possible on  $Ni_{61}Pt_{39}$  NPs than on Pd NPs, as observed in Table 1. On the other hand, Wilson and Flaherty<sup>36</sup> proposed another mechanism for H<sub>2</sub>O<sub>2</sub> formation on Pd NPs called a heterolytic reaction mechanism, similar to the twoelectron ORR, in which an electron is generated during the

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**Fig. 4 Characterizations of the synthesized bimetallic NPs.** XRDs for a  $Au_{51}Pd_{49}$ , b  $Ni_{61}Pt_{39}$ , c  $Pd_{50}Cu_{50}$ , d  $Pd_{52}Ni_{48}$ , e  $Pt_{58}Co_{42}$ , f  $Pt_{52}Pd_{48}$ , g  $Rh_{56}Ni_{44}$ , h  $Rh_{56}Pt_{44}$  NP samples. For comparison, the red and green lines in the XRD patterns correspond to the peaks of pure elements in each bimetallic NP. The blue peaks were simulated with the crystal structures of the bimetallic system predicted by DFT calculations. Above each XRD pattern, the element mapping images acquired by STEM-EDX are included, where the first image (the most left) is the overlay image of the maps for elements in each bimetallic NP. The scale bars correspond to 20 nm. The enlarged images of the STEM-EDX are also provided in Supplementary Figures 2~9.

oxidation process of H<sub>2</sub> on the NP surfaces. We also investigated the mechanism on Ni<sub>50</sub>Pt<sub>50</sub>(111) and Pd(111) by DFT calculations where the computational hydrogen electrode method was used along with consideration of implicit water solvents (Fig. 5b). On both Pd(111) and Ni<sub>50</sub>Pt<sub>50</sub>(111), the ORR processes for H<sub>2</sub>O<sub>2</sub> formation are thermodynamically favorable. In particular, although the first protonation is very similar (-1.03 eV for Pd and -1.00 eV for Ni<sub>50</sub>Pt<sub>50</sub>(111) (-1.40 eV vs -1.58 eV). This mechanism also readily reveals more preferential H<sub>2</sub>O<sub>2</sub> production on Ni-Pt surfaces than on Pd surfaces.

In Fig. 5a, it is interesting that  $Ni_{50}Pt_{50}(111)$  stabilizes  $H_2O_2^*$  (III state) more than Pd(111) does, whereas the energetics for OOH\* (II state) are comparable on the two surfaces. To clarify this result, we investigated the binding characteristics between the adsorbates (OOH\* and  $H_2O_2^*$ ) and catalyst surfaces (e.g., Pd(111) and  $Ni_{50}Pt_{50}(111)$ ) via projected crystal orbital Hamilton population (pCOHP) analysis (Supplementary Figure 15a), in which we display the pCOHPs according to the typical method, namely drawing negative (i.e., bonding) contributions to the right and positive (i.e.,

anti-bonding) contributions to the left. For OOH\* binding to Pd (111) and Ni<sub>50</sub>Pt<sub>50</sub>(111), the bonding contributions are comparable. In other words, there are three energy windows for the bonding contributions: -3 to -4 eV (1st window), -5 to -7 eV (2nd), and -8 to -9 eV (3rd). Here, the bonding energy levels for the first and third contributions are lower (stronger binding) for Ni<sub>50</sub>Pt<sub>50</sub>(111), whereas the bonding energy levels for the second are lower for Pd(111). On the other hand, in the case of  $H_2O_2^*$ binding, all of the bonding contributions for  $Ni_{50}Pt_{50}(111)$  are lower than those for Pd(111), which explains why the  $H_2O_2^*$ adsorbate is more stable on Ni<sub>50</sub>Pt<sub>50</sub>(111) than Pd(111). This behavior can be explained by the back-bonding character between H<sub>2</sub>O<sub>2</sub>\* and Ni<sub>50</sub>Pt<sub>50</sub>(111). Alloying of Pt and Ni creates electron-rich Ni atoms in the alloy structure, which leads to backbonding with the adsorbate (the Ni atom donates electrons to an empty orbital in the adsorbate). This effect is significantly enhanced for H2O2\* compared to OOH\* as the O atom in the adsorbate bonded to metal surfaces is more electron-deficient for  $H_2O_2^*$  than OOH\* due to the additional O-H bond in  $H_2O_2^*$ . From the charge density difference plot shown in Supplementary Figure

Table 1. Catalytic performances of eight dimetallic NPs proposed by the DF1 screening process in comparison with that of pure Pd NPs.					
Catalyst	H <sub>2</sub> O <sub>2</sub> productivity			H <sub>2</sub> conversion (%)	H <sub>2</sub> O <sub>2</sub> selectivity (%)
	Mass-normalized (mmol/g <sub>metal</sub> ·h)	Cost-normalized (mmol/\$ <sub>metal</sub> ·h)	TOF (h <sup>-1</sup> )		
Au <sub>51</sub> Pd <sub>49</sub> (1.43) <sup>a</sup>	505.2	7.1	77.1	11.6	70.1
Ni <sub>61</sub> Pt <sub>39</sub> (1.16)	880.1	69.3	98.5	22.9	61.2
Pd <sub>50</sub> Cu <sub>50</sub> (1.51)	49.4	1.3	4.2	1.6	50.8
Pd <sub>52</sub> Ni <sub>48</sub> (0.84)	218.1	5.5	18.2	2.8	>99.9 <sup>b</sup>
Pt <sub>58</sub> Co <sub>42</sub> (1.78)	87.6	4.6	12.1	11.0	12.8
Pt <sub>52</sub> Pd <sub>48</sub> (1.16)	1225.6	23.0	186.9	25.0	78.7
Rh <sub>56</sub> Ni <sub>44</sub> (0.98)	16.8	0.1	1.4	-	-
Rh <sub>56</sub> Pt <sub>44</sub> (1.67)	109.3	0.6	15.7	10.6	16.6
Pd	552.4	7.3	58.8	14.0	63.0

aT

<sup>b</sup>The high selectivity is mainly caused by the low  $H_2$  conversion property.

15b, we find that Ni atoms on  $Ni_{50}Pt_{50}$  and O atoms in  $H_2O_2^*$ donate electrons (cyan isosurface) while the O atoms in  $H_2O_2^*$  also accept electrons (yellow), indicating the back-bonding mode between the metal and  $H_2O_2$ .

In addition, we discuss the selectivity of H<sub>2</sub>O<sub>2</sub> production on Pd (111) and Ni<sub>50</sub>Pt<sub>50</sub>(111) with DFT calculations. It is well known that  $H_2O$  production, the side reaction for  $H_2O_2$  production, occurs by the O-O bond dissociation<sup>27,32-34</sup>. Therefore, we investigated the possible O-O bond scission reactions on the Pd(111) and Ni<sub>50</sub>Pt<sub>50</sub>(111) surfaces by DFT calculations, where we considered the ratio of the O-O bond dissociation barrier at several steps to the corresponding hydrogenation step barrier or desorption barrier ( $O_2^*$  dissociation vs  $O_2^*$  hydrogenation, OOH\* dissociation vs OOH\* hydrogenation, and  $H_2O_2$  dissociation vs  $H_2O_2^*$ desorption) for  $H_2O_2$  production as an estimation for the  $H_2O_2$ selectivity (Supplementary Table 5). We assume that the H<sub>2</sub>O production reaction occurs most frequently at the O-O bond scission step with the lowest reaction barrier among the three possible O-O bond scission reactions. Comparing the ratios for the three O-O bond scission reactions, Pd(111) shows the lowest ratio of 0.14 (unitless) at the  $H_2O_2^*$  scission step, which is similar to that of Ni<sub>50</sub>Pt<sub>50</sub>(111) (0.12 at the OOH\* scission step). This is consistent with the experimental finding that the selectivity for  $H_2O_2$ production is similar for both Pd (63.0%) and Ni<sub>50</sub>Pt<sub>50</sub> (61.2%).

#### DISCUSSION

This work demonstrates an efficient computational-experimental screening protocol for the development of bimetallic catalysts to replace conventional Pd catalysts for H<sub>2</sub>O<sub>2</sub> direct synthesis. Using this protocol, a Pd-free bimetallic catalyst, Ni<sub>61</sub>Pt<sub>39</sub>, was successfully developed. Here, we note that Ni and Pt have not usually been considered in the catalysis field for H<sub>2</sub>O<sub>2</sub> direct synthesis because they prefer to dissociate  $O_2$  molecules, which prevents H<sub>2</sub>O<sub>2</sub> formation, although Ni-Pd<sup>25</sup>, Pt-Pd<sup>26</sup>, and Pt-Ag<sup>37</sup> bimetallic catalysts have been reported. The success story of our protocol primarily results from the validity of our descriptor, the similarity of electronic DOS patterns, for catalyst screening. Moreover, one can readily extend our screening protocol by updating a reference material. For example, since the Ni-Pt system shows superior catalytic performance in this work, we can discover other catalysts by using the DOS pattern of the Ni-Pt alloy as a reference, which remains as future work. In this regard, this protocol will immediately provide opportunities for catalyst discovery for the replacement or reduction in the use of the platinum-group metals and then enable the further application of these catalysts to other chemical reactions.

## **METHODS**

### Computational details for screening bimetallic catalysts

We generated 10 ordered phases for each bimetallic alloy with a 1:1 composition. Specifically, the crystal structure prototypes were obtained by NaCl (B1), CsCl (B2), zinc blende (B3), wurtzite (B4), TiCu (B11), CdAu (B19), FeB (B27), CrB (B33), AuCu (L1<sub>0</sub>), and CuPt (L1<sub>1</sub>) compounds from the Material Project<sup>38</sup>. Here, the initial lattice parameters were replaced by values commensurate with covalent radii of two elements in the target compounds. By means of the DFT optimization process, we collected the most stable bulk phases of 4350 binary alloys. Furthermore, the formation energies ( $\Delta E_f$ ) of all the bulk phases were calculated as follows:  $\Delta E_f = E$ [AB] - E[A] - E[B], where E[AB], E[A], and E[B] are the total energies of the bimetallic AB compound, A crystal, and B crystal in the unit cell. For thermodynamically favorable alloys, a close-packed surface of each crystal structure was used for the calculation of the DOS pattern of each alloy. In principle, the close-packed surface of L10 is the (111) facet, that of B2 is the (110) facet, and those of other crystal structures are the (001) facet<sup>39</sup>. The DOS patterns were obtained by the sum of the partial DOSs on the surface atoms.

To investigate thermodynamic stabilities in bulk phases and the DOS patterns of surface atoms, spin-polarized DFT calculations were performed using the Vienna Ab Initio Simulation Package (VASP)<sup>40</sup> with projectoraugmented-wave (PAW) pseudopotentials<sup>41</sup> and the revised Perdew-Burke-Ernzerhof (RPBE) exchange-correlation functional<sup>42</sup>. Then, we used a plane-wave kinetic energy cutoff of 400 eV and Monkhorst-Pack k-point meshes of  $8 \times 8 \times 8$  for the bulk systems and  $4 \times 4 \times 1$  for the slab systems. The bulk of the  $1 \times 1 \times 1$  unit cell and the slab of the  $2 \times 2$  unit cell with four layers were used. In the slab systems, a vacuum spacing of 15 Å was used to avoid interactions between slabs. All relaxations were performed until the energy change was  $>1 \times 10^{-6}$  eV/cell and the forces on the individual atoms were <0.01 eV Å<sup>-1</sup>.

#### H<sub>2</sub>O<sub>2</sub> formation mechanism

The energy diagrams for  $H_2O_2$  production on the  $Ni_{50}Pt_{50}(111)$  surface and Pd(111) surfaces were also calculated by the DFT method. The simulations were performed using the VASP<sup>40</sup> using the PAW<sup>41</sup> pseudopotentials to describe the potential from the ionic core. For the exchange and correlation terms, we employed the RPBE functional<sup>42</sup> with Grimme's D3 dispersion correction<sup>43</sup>. An energy cutoff of 400 eV and Monkhorst-Pack k-point meshes of  $3 \times 3 \times 1$  for the slab calculations were used. A large vacuum spacing of 15 Å was used to prevent interslab interactions. The top two layers and the reactant molecules were optimized until the energy change was  $<1 \times 10^{-4}$  eV/cell and the force on each atom was less than 0.02 eV Å<sup>-1</sup>. In the case of the Langmuir-Hinshelwood mechanism, the climbing image nudged elastic band<sup>44</sup> method was employed to investigate the transition states for the main reaction. For the electron-proton transfer mechanism, the computational hydrogen electrode method<sup>45</sup> with U = 0 V in addition to the water solvation energy calculated with the implicit solvent model implemented within the VASP<sub>sol</sub> package<sup>46</sup> was used to construct the energy diagram



Fig. 5  $H_2O_2$  direct synthesis mechanisms of Ni<sub>50</sub>Pt<sub>50</sub>(111) and Pd(111) from DFT calculations. a The Langmuir-Hinshelwood mechanism. b The electron–proton transfer mechanism. The cyan lines are the energy diagram for Ni<sub>50</sub>Pt<sub>50</sub>(111), and the magenta lines are for Pd(111). The color code for the atoms is as follows: teal = Ni, coral = Pt, red = O, and green = H.

on the following reactions:

 $O_{2(g)} \rightarrow *O_2$  (3)

$$*O_2 + H^+ + e^- \to *OOH \tag{4}$$

 $*OOH + H^+ + e^- \rightarrow *H_2O_2 \tag{5}$ 

$$*H_2O_2 \to H_2O_{2(q)} \tag{6}$$

We also performed pCOHP calculations<sup>47</sup> using the LOBSTER package<sup>48</sup> to understand the binding character between the adsorbates (e.g., OOH\* and  $H_2O_2^*$ ) and catalyst surfaces (e.g., Pd(111) and Ni<sub>50</sub>Pt<sub>50</sub>(111)). The differential charge density ( $\Delta\rho$ ) of the  $H_2O_2^*$  adsorbates on the Ni<sub>50</sub>Pt<sub>50</sub> (111) surface was evaluated by the following:

$$\Delta \rho = \rho_{\rm tot} - \rho_{\rm ads} - \rho_{\rm slab} \tag{7}$$

where,  $\rho_{tot}$  is the charge density of the  $H_2O_2^{*}-Ni_{50}Pt_{50}$  system and  $\rho_{ads}$ , and  $\rho_{slab}$  are the charge densities of the  $H_2O_2^{*}$  adsorbate and metal slab, respectively. The atomic coordinates for  $\rho_{ads}$ , and  $\rho_{slab}$  are equal to those in the  $H_2O_2^{*}-Ni_{50}Pt_{50}$  system.

#### Chemicals

Palladium(II) acetate [Pd(CH<sub>3</sub>COO)<sub>2</sub>,  $\geq$ 99.9%], copper(II) acetate [Cu (CH<sub>3</sub>COO)<sub>2</sub>, 99.99%], nickel(II) acetylacetonate [Ni(acac)<sub>2</sub>, 95%], rhodium (III) nitrate hydrate [Rh(NO<sub>3</sub>)<sub>3</sub>:XH<sub>2</sub>O, ~36%], gold(III) chloride trihydrate [HAUCI<sub>4</sub>:3H<sub>2</sub>O, 99.9%], chloroplatinic acid hydrate [H<sub>2</sub>PtCI<sub>6</sub>:XH<sub>2</sub>O, ~38%], cobalt acetate tetrahydrate [Co(CH<sub>3</sub>COO)·4H<sub>2</sub>O, 99.999%], dioctyl ether, oleylamine, and n-butyllithium solution [2.0 M in cyclohexane] were purchased from Sigma-Aldrich. Ethanol was analytical grade and was used without further purification.

## **Catalyst synthesis**

All alloy metal catalysts and Pd catalysts were synthesized using the butyllithium reduction method. To synthesize the bimetallic XY catalysts, 0.017 mmol of X precursor and Y precursor (details are described in Table 3 of Supporting Information) were dissolved in 10 mL of dioctyl ether with 2 mL of oleylamine at 50°C. The solution was then injected into a butyllithium solution containing 15 mL of dioctyl ether and 1.2 mL of 2.0 M butyllithium in cyclohexane at 50°C for 1.5 h in an Ar atmosphere. The reaction mixture was further heated to 260°C for 1 h. The mixture was cooled to room temperature, and 1.25 mL of trioctylphosphine was

injected to protect the colloids. The resulting NPs were washed with ethanol three times.

## Catalyst characterization

Transmission electron microscopy (TEM) images and energy-dispersive Xray spectra (EDS) were acquired using a transmission electron microscope (FEI Talos F200X) equipped with scanning transmission electron microscopy-energy dispersive X-ray spectroscopy (Bruker Super-X EDS system). The crystal structure was examined by X-ray diffraction (Rigaku Dmax 2500) with Cu Ka radiation ( $\lambda = 1.5406$  Å). The samples for the TEM images and X-ray diffraction patterns were purified by centrifugation three times to remove the surfactants and/or excess reactants. Then, the NPs were dispersed in ethanol. The resulting solution was dropped on a copper grid coated with an amorphous carbon film for the TEM images and a soda-lime-silica glass for the X-ray diffraction pattern. The actual compositions of each alloy catalyst were measured via ICP atomic emission spectrometry using iCAP6500 Duo (Thermo).

#### **Catalyst performance measurements**

The direct synthesis of  $H_2O_2$  was performed in a double-jacket glass reactor under stirring at 1200 rpm. The reaction medium (150 ml) was composed of ethanol and water (ethanol:water volume ratio = 1:4) with 0.9 mM sodium bromide (NaBr) and 0.02 M phosphoric acid ( $H_3PO_4$ ). The catalyst weight used was 1 mg. The volumetric flow rate of the reactant gas stream was 22 ml/min ( $H_2:O_2$  volume ratio = 1:10). The reaction was performed at 293 K and 1 atm for 1 h. After the reaction, the concentration of  $H_2O_2$  was calculated using gas chromatography (Younglin, 6500GC) equipped with a Molecular Sieve 5 A (Supelco, 60/80 mesh, 6 ft × 1/8 in, 2.1 mm) packed column and a thermal conductive detector. The catalytic properties ( $H_2O_2$  productivity,  $H_2$  conversion, and  $H_2O_2$  selectivity) shown in Table 1 were calculated with the following equations:

$$H_2 \text{ conversion}(\%) = \frac{\text{moles of reacted } H_2}{\text{moles of supplied } H_2} \times 100$$

$$H_2O_2 \text{ selectivity}(\%) = \frac{\text{moles of formed } H_2O_2}{\text{moles of reacted } H_2} \times 100$$

$$H_2O_2 \text{ productivity}(mmol/g_{metal}nh) = \frac{mmoles \text{ of formed } H_2O_2}{\text{weight of metal}(g) \times \text{ reaction time}(h)}$$

$$TOF(h^{-1}) = \frac{\text{mmoles of formed } H_2O_2}{\text{mmols of metal} \times \text{reaction time}(h)}$$

## DATA AVAILABILITY

All data needed to evaluate the conclusions of this paper are available within the paper and Supplementary Information.

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## AUTHOR CONTRIBUTIONS

S.S.H. conceived the idea. B.C.Y., Hyunji Nam, S.Y.L., and S.S.H. designed the calculations and experiments. B.C.Y. performed the high-throughput DFT calculations. Hyunji Nam and Hyobin Nam performed the synthesis and characterization of NP catalysts. Hyunji Nam, Hyobin Nam, K.-Y.L., S.-C.K., and S.O.W. performed the catalytic performance measurements. M.-C.K, H.W.L., and D.K. performed DFT calculations on the catalytic reaction mechanism. B.C.Y., Hyunji Nam, M.-C.K., H.W.L., S.Y.L., and S.S.H.

analyzed and discussed the results. B.C.Y., Hyunji Nam, M.-C.K., S.Y.L., and S.S.H. drafted the manuscript. S.Y.L. and S.S.H. supervised the research. All the authors approved the final version of the manuscript. B.C.Y. and Hyunji Nam contributed equally to this work.

### COMPETING INTERESTS

The authors declare no competing interests.

#### ADDITIONAL INFORMATION

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